



## Solidification enhancement of phase change material in a triplex tube latent heat energy storage unit using longitudinal-parabolic fins

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**ABSTRACT:** This paper numerically investigates the solidification performance improvement of phase change material in a triplex tube latent heat thermal energy storage unit by introducing an innovative longitudinal-parabolic fin. A numerical model based on the enthalpy-porosity approach is employed to simulate the discharging process. Simulation results reveal that the longitudinal-parabolic fins outperform the conventional straight fins in effectually increasing the phase change performance of the latent heat thermal energy storage unit. The complete discharging time of the triplex tube latent heat thermal energy storage unit with the proposed fin was reduced by up to 38.5% compared to that of the unit with straight fins. The study also investigates the influence of geometric parameters of the designed fin to achieve superior phase change material discharging efficiency. Effects of radial pitch and angular pitch of the longitudinal-parabolic fins on energy discharge time are studied by examining various cases under the constant total fins volume. Results infer that the radial pitch of parabolic fins has a moderate impact on solidification time improvement, while the angular pitch has a remarkable impact on reducing energy discharging time. Decreasing the angular pitch from 120° to 60° reduces the solidification time by 52.3%. The maximum of saving discharge time for the most efficient fin design is 61.8% in comparison with straight fins.

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### 1- Introduction

The increasing energy demand has led researchers to focus on effectively harnessing renewable energy sources and optimizing current energy systems. Thermal energy is obtained from different renewable energy resources like solar, nuclear power, and geothermal. Most renewable energy resources suffer from the drawback of inferior stability, which makes thermal energy storage crucial for effectively harnessing renewable energy. Thermal energy is stored in the form of thermo-chemical heat, sensible heat, or latent heat. Latent heat thermal energy storage is preferred over sensible heat storage owing to its higher storage capacity, compactness, and constant temperature operation [1-3].

Latent heat thermal energy storage systems (LHTES) employ phase change material (PCM) to store and release a high amount of thermal energy when undergoing phase transition [4,5]. However, LHTES systems pose major challenges due to the inferior thermal conductivity of PCMs that hampers the rate of phase change [6,7]. Thermal performance enhancement of LHTES systems is performed through various techniques, including the use of nanoparticles [8-11], metal foam [12-14], fins [15-17], and composite phase change materials [18,19]. Among these methods, adding high-conductive fins has emerged as the most prevalent

approach for the effective enhancement of energy storage efficiency [20]. Various configurations of fins have been presented in the literature with different parameters that have been adjusted to find the optimal configuration to increase heat transfer in LHTES systems. Sciacovelli et al. [21] introduced a Y-shaped fin design to increase the efficiency of the LHTES system and found that these fins are more efficient than straight fins. They optimized the configuration of fins by a combination of the response surface method and CFD simulation and observed that the efficiency improved by adding the bifurcations in the fins. Sheikholeslami et al. [22] designed a new fin based on the snowflake structure. Their finding demonstrates that the inclusion of snowflake-shaped fins accelerates the discharging process of the storage unit up to 1.5 times when compared to straight fins. Aly et al. [23] analyzed the potential of longitudinal corrugated fins for increasing the PCM discharging rate in the LHTES unit. Numerical findings demonstrated that corrugated fins shortened the full discharging time up to 30-35% in comparison with straight fins. Zhang et al. [24] proposed helical fins to accelerate the PCM charging rate in thermal energy storage systems. They found that the best thermal performance in vertical LHTES can be achieved by a double helical fin, and in a horizontal LHTES with a quadruple helical fin. Compared with traditional longitudinal fins, the total charging time declined up to 31% and 10% in vertical

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and horizontal systems. Huang et al. [25] studied the melting/solidification process of the LHTES unit equipped with fractal tree-shaped fins. Numerical findings revealed that the full PCM melting and solidification times declined up to 34.5% and 49.4% compared to rectangular fins. Yao and Huang [26] proposed longitudinal triangular fins to enhance the discharging performance of the triplex-tube TES system. They concluded that the solidification time decreased up to 30.98% compared to typical rectangular fins. Huang and Yao [27] proposed a new trapezoidal longitudinal outer fin distributed by the Fibonacci sequence and analyzed the effect of different longitudinal fin arrangements on solidification performance. Numerical results illustrated that the discharging time using a modified trapezoidal fin is shortened up to 45.28% compared with the quadrilateral fin. Patel et al. [28] studied PCM's heat transfer enhancement using combined eccentricity and longitudinal fin. Among the eccentricities of -15mm to +15mm, the most effective eccentricities were +10mm in melting and -3mm in solidification with 27.63% and 12.82% reduction in phase change time, respectively. Zheng et al. [29] proposed an arrow-shaped fin structure based on a fast optimization algorithm to increase the discharging performance of the LHTES system. Results showed the arrow-shaped fins could decrease the full solidification time up to 52% compared to the traditional Y-shaped fins. Lijun et al. [30] investigated the discharging efficiency enhancement of LHTES devices using an eccentric fractal finned tube and concluded that the complete discharging time declined up to 41.2% compared with eccentric rectangular fins. Zhang et al. [31] proposed the combination of novel branch-structured fins and nanoparticles to enhance the solidification performance of PCM in a triple-tube heat exchanger. They concluded that the discharging time is reduced up to 10.3% for nanoparticles only and 83% for fin only. Ma Zhang et al. [32] summarized the research on the heat transfer improvement of PCM using fin tubes. They compared different fin structures including rectangular fin, spiral fin, annular fin, plate-fin, and dendritic fin. They found that rectangular fins usually show better performance than annular fins and innovative fins are generally better than rectangular fins. Amini and Abbasirad [33] proposed an innovative longitudinal arc fin to increase the charging efficiency of LHTES devices. Numerical results demonstrated that the optimized fin configuration declined the full charging time by 67.7% compared to rectangular fins. Li et al. [34] worked on the influence of leaf-shaped longitudinal fins on the charging efficiency of PCM-based shell and tube storage devices. They evaluated the influences of fin geometry parameters and showed that by increasing the sub-branch length of leaf-shaped fins, the charging process accelerated, and more uniform heat transfer achieved. Tavakoli et al. [35] proposed sinusoidal fins for performance improvement of LHTES system. They conducted a comprehensive sensitivity analysis and observed that the melting rate accelerated up to 62% in comparison with straight fins. Oskouei and Bayer [36] executed experimental and numerical studies on energy storage improvement in a LHTES system using Fibonacci-inspired fins. Their results inferred that the complete

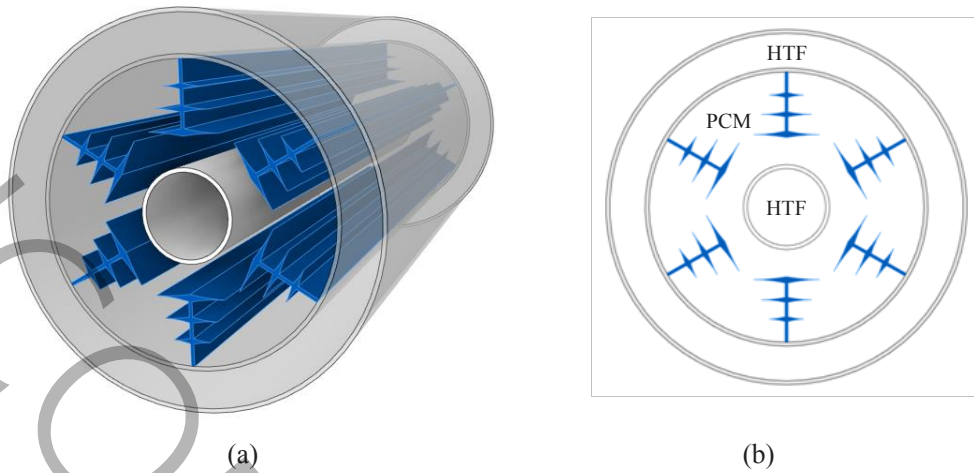
solidification and melting time declined up to 45% and 20% in comparison with longitudinal fins. Zheng et al. [37] designed a spiderweb-shaped fin for energy release improvement of LHTES unit. They optimized the geometrical parameters of the proposed fin and found that the full discharging time decreased by up to 88.9% compared to rectangular fins. Boujelbene et al. [38] explored the impact of twisted fins on PCM melting and solidifying rates in a LHTES system and demonstrated the melting and solidification rates by twisted fins improved by 10% and 14% in comparison with straight fins. Li et al. [39] employed structural-optimized spiral fins to increase the performance of heat storage in LHTES unit. Numerical results illustrated that a thermal storage system with a denser, higher, and thicker bottom fin demonstrates a faster charging rate.

After conducting a thorough literature review, it is apparent that altering the fins configuration could effectively improve the thermal performance of LHTES systems and significant achievements have been made in practical applications. Nevertheless, there is still much space for further improvement in the energy storage performance of LHTES units by exploring more innovative fin configurations. This paper innovatively presents a new longitudinal-parabolic fin and conducts a detailed numerical investigation to explore the influences of different geometrical parameters of the designed fin on the discharging efficiency of the PCM in a triplex tube LHTES unit. The longitudinal-parabolic fin will be evaluated against the conventional straight fin to find out the superior thermal performance of the innovative fin. While the total surface area of fins is kept constant, several cases with different fin's geometric parameters including radial pitch and angular pitch are designed to determine the most efficient fin layout to achieve the highest thermal energy release efficiency.

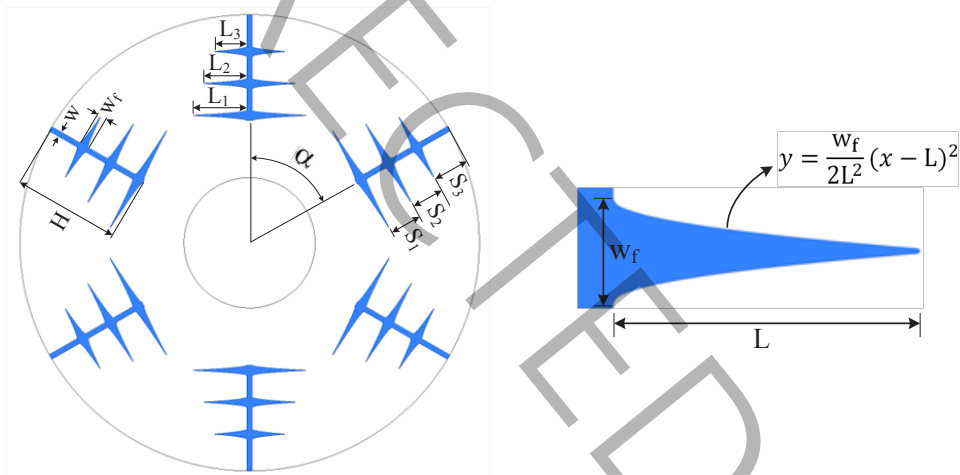
## 2- Model description

The physical model entails a PCM-based triplex tube LHTES unit with longitudinal-parabolic fins, as depicted in Fig. 1. The water as HTF passes in the inner tube and in the region between the middle and outer tubes, and the PCM is filled in the annulus region among the inner and middle tubes. The computational domain is regarded as a two-dimensional model due to the smaller temperature gradient in the axial direction than in the radial direction. The space among the inner and middle tubes of the storage system is the simplified domain for the simulation (Fig. 1(b)). The diameters of the inner and middle tubes are 20 mm and 70 mm, respectively. The solid material for the tubes and fins is copper and RT35 is chosen as the PCM. The thermophysical properties of the involved materials are displayed in Table 1 [40].

The longitudinal-parabolic fins are designed to increase the efficiency of the PCM-based thermal energy storage unit during the discharge phase. The proposed fin consists of a quadrilateral fin as the base of the structure and three parabolic sub-fins with different heights that are connected to the base fin. To assess the longitudinal-parabolic fins, their thermal performances are compared to those of traditional



**Fig. 1. The triplex tube LHTES unit: (a) 3D schematic view, (b) 2D cross section.**



**Fig. 2. Two-dimensional computational domain.**

straight fins. The influence of geometrical parameters of longitudinal-parabolic fins including radial pitch (space between sub-fins in the radial direction) and angular pitch (the angle between two fins in the circumference direction) are evaluated. Nine different cases are analyzed in this study. The fins are designed so that the total cross-section area remains fixed in all cases to enable the comparability of the system with different fin configurations. Accordingly, the amount of PCM remains constant in all cases. Fig. 2 depicts the geometrical parameters of the longitudinal-parabolic fins including length ( $H$ ) and width of the quadrilateral fin ( $w$ ), heights ( $L_1, L_2, L_3$ ), root width ( $w_f$ ) and radial pitches ( $S_1, S_2, S_3$ ) of the parabolic sub-fins, and angles between the fins ( $\alpha$ ). The parabolic equation of sub-fins is also shown

in Fig. 2. The coefficient  $w_f / 2L^2$  determines the steepness and direction of the parabola. The value of  $\alpha$  influences how wide or narrow the parabola is. The details of the geometrical characteristics for each case are listed in Table 2.

### 3- Mathematical modeling

#### 3- 1- Governing equations and numerical implementation

PCM solidification process was numerically simulated via the enthalpy-porosity method [41]. This method does not explicitly track the common solid-liquid interface, rather the computational region is considered to be a porous zone. The porosity is identical to the PCM liquid fraction which is calculated using the enthalpy balance, and changes from zero to one in the mushy zone. The following assumptions were

**Table 1. Thermo-physical properties [40]**

Properties	Materials	
	Paraffin (RT35)	Copper
Name, Symbol (unit)		
Liquidus Temperature, $T_l$ (K)	308	–
Solidus Temperature, $T_s$ (K)	302	–
Density, liquid, $\rho_l$ (kg/m <sup>3</sup> )	880	–
Density, solid, $\rho_s$ (kg/m <sup>3</sup> )	760	8798
Specific heat, liquid, $C_{pl}$ (J/kgK)	1800	–
Specific heat, solid, $C_{ps}$ (J/kgK)	2400	381
Thermal conductivity, $k$ (W/mK)	0.2	387.6
Dynamic viscosity, $\mu$ (kg/ms)	0.023	–
Latent heat of fusion, $L_f$ (J/kg)	170000	–
Thermal expansion Coefficient, $\beta$ (1/K)	0.0006	–

**Table 2. Geometric dimensions of all cases (all dimensions are in mm.).**

Case	$H$	$w$	$w_f$	$L_1$	$L_2$	$L_3$	$S_1$	$S_2$	$S_3$	$\alpha^\circ$
Base Case	20	2.75	-	-	-	-	-	-	-	90
Case 1	20	1	2	10	8	6	6	6	8	90
Case 2	20	1	2	10	8	6	4	4	12	90
Case 3	20	1	2	10	8	6	6	4	10	90
Case 4	20	1	2	10	8	6	10	4	6	90
Case 5	20	1	2	10	8	6	4	10	6	90
Case 6	20	1	2	10	8	6	6	10	4	90
Case 7	22	1.16	2.3	12	9	7	7	7	8	120
Case 8	16	0.8	1.5	8	6	4	5	5	6	60

considered for the numerical simulation:

- The flow of PCM is transient, incompressible, and laminar.
- The PCM's thermophysical properties, except for its density, are considered temperature-independent.
- The PCM's volume change caused by phase transition is neglected.
- Temperature changes in the HTF are neglected.
- Boussinesq approximation is employed for the buoyancy effect.
- Heat loss to the environment is insignificant.

The equations governing the PCM solidification process are defined by continuity, momentum, and energy equations [42]:

$$\frac{\partial u_i}{\partial x_i} = 0 \quad (1)$$

$$\rho \frac{\partial u_i}{\partial t} + \rho \frac{\partial u_i u_j}{\partial x_j} = -\frac{\partial p}{\partial x_i} + \mu \frac{\partial^2 u_i}{\partial x_j^2} + \rho \beta (T - T_{ref}) g_i + S_i \quad (2)$$

$$\rho \frac{\partial H}{\partial t} + \rho \frac{\partial u_i H}{\partial x_i} = \frac{\partial}{\partial x_i} k \frac{\partial T}{\partial x_i} \quad (3)$$

where  $u_i$ ,  $\rho$ ,  $\mu$ ,  $p$ ,  $g_i$ ,  $k$  and  $T$  are fluid velocities, density, dynamic viscosity, pressure, gravity, thermal conductivity, and temperature. The total enthalpy ( $H$ ) of PCM is given by:

$$H = h + \Delta H \quad (4)$$

$$h = \int_{T_{ref}}^T C_p dT + h_{ref} \quad (5)$$

in which  $h_{ref}$  is the sensible enthalpy corresponding to the reference temperature  $T_{ref}$ , and  $C_p$  indicates the specific heat capacity. The latent heat is stated as:

$$\Delta H = \lambda L_f \quad (6)$$

where  $L_f$  refers to the latent heat.  $\lambda$  is the melting fraction expressed as:

$$\lambda = \begin{cases} 0 & \text{if } T \leq T_s \\ \frac{T - T_s}{T_l - T_s} & \text{if } T_s < T < T_l \\ 1 & \text{if } T \geq T_l \end{cases} \quad (7)$$

The subscripts ' $l$ ' and ' $s$ ' indicate the PCM liquidus and solidus states, respectively. The momentum source term  $S_i$  is defined as [43]:

$$S_i = A_m \frac{(1 - \lambda)^2}{\lambda^3 + \varepsilon} u_i \quad (8)$$

Where  $A_m$  is the mushy constant which varies from  $10^4$  to  $10^7$ , and is set to  $10^5$  in this study [44].  $\varepsilon$  Represents a small value to avoid zero denominators when  $\lambda = 0$ .

Ansys-Fluent software is applied for numerical simulations. The finite volume method with a transient pressure-based solver is applied. The momentum and energy equations are discretized using the QUICK scheme. The PRESTO algorithm is used for the pressure correction equation. The SIMPLE scheme is applied to couple the pressure and velocity. The relaxation factors for pressure, momentum, liquid fraction, and energy are 0.3, 0.7, 0.9, and 1, respectively. The convergence criterion was set at  $10^{-4}$  in the continuity and momentum equations, and  $10^{-6}$  in the energy equation.

### 3- 2- Boundary and initial conditions

At the onset of the discharging process, the temperature of the system is initialized as 320 K. The surfaces of both inner and outer tubes are maintained at a constant temperature at 250 K which is lower than the PCM solidus temperature. Moreover, a no-slip condition was imposed at the walls.

### 3- 3- Grid and time step independence study

Grid independence in the numerical solution was examined through different grid sizes and the result is shown in Fig. 3(a). An unstructured grid was adopted for better compatibility. The complete solidification time for six different grids with 41371, 57522, 103451, 233530, 361045, and 527092 cells were studied. The results illustrated that increasing the elements number from 103k to 527k does not result in considerable variation in the outcomes. Hence, a grid size of 103451 elements was selected to consider solution accuracy and computational time. The generated grid is shown in Fig. 3(b).

Time step independence analysis was also investigated. Fig. 4 shows the complete solidification time and solid fraction among different time steps. It is apparent that the solid fraction curves are almost identical for time steps less than 0.2s. Thus, to efficiently save computational cost and accurate prediction, the time step of 0.2s is assumed for the next simulations.

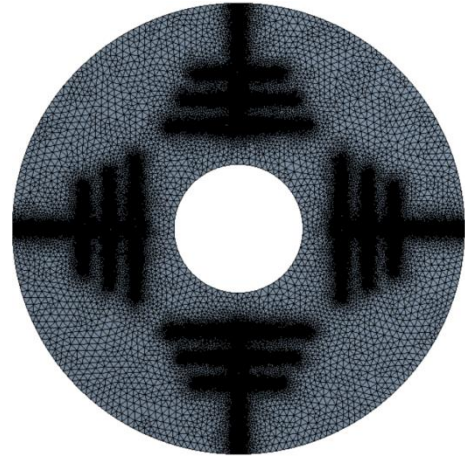
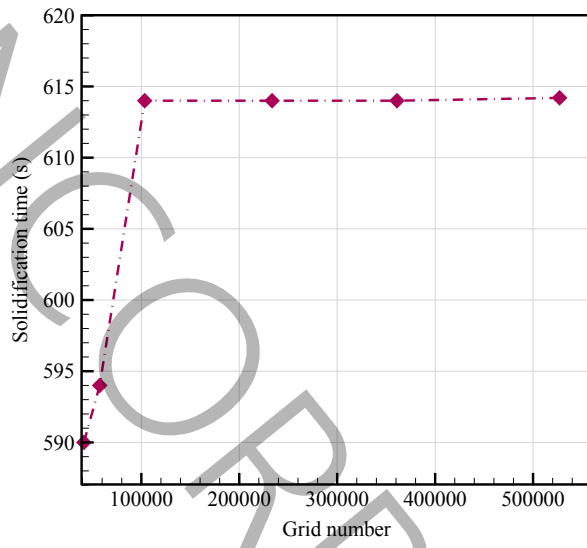
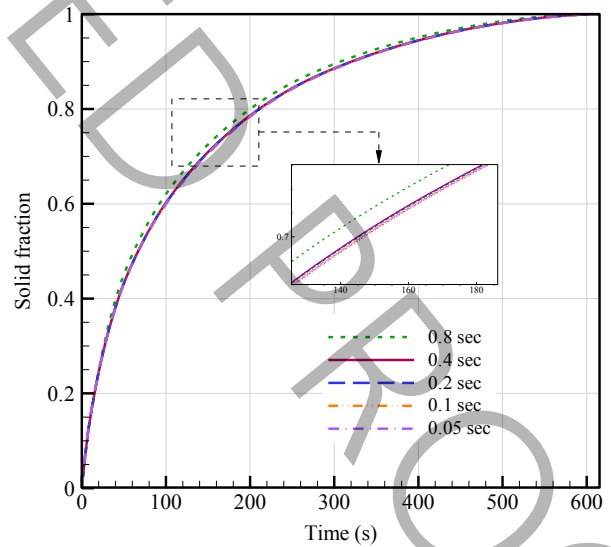
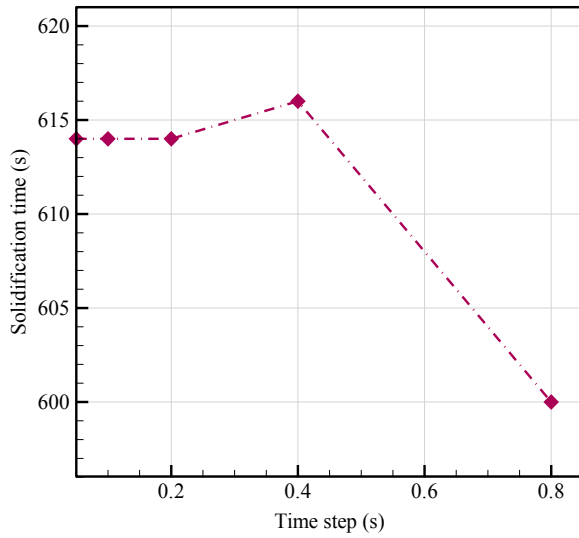


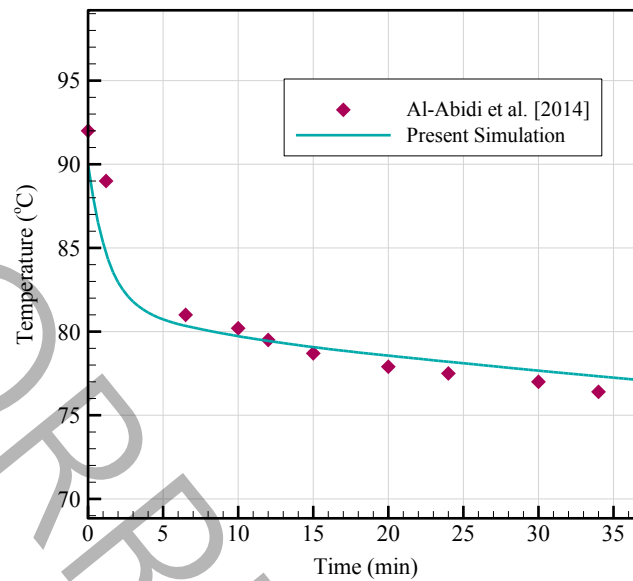
Fig. 3. (a) Grid size independence verification, (b) the computational grid.



(a)

(b)

Fig. 4. Time step independence study.



**Fig. 5. Comparing numerical predictions with experimental work in [45].**

### 3- 4- Numerical modeling validation

The current numerical approach has been validated through a comparison of the simulation results with experimental analysis carried out by Al-Abidi et al. [45]. In their experiment, the PCM phase change process in a thermal storage enclosure with straight fins was studied. Fig. 5 shows a comparison of the PCM mean temperature throughout the discharging process for the numerical prediction and experimental data. The comparison indicates that the current prediction agrees well with the reference work. The maximum relative error between the numerical prediction and the experimental measurements is 5%, which verifies the current numerical approach.

## 4- Results and discussion

Numerical simulation results are presented in four subsections. The first subsection compares the performance of longitudinal-parabolic fins and conventional straight fins. The second subsection investigates the impact of fin radial pitch on the PCM discharging process. The third subsection examines the effect of angular pitch on solidification performance. The fourth subsection compares the full solidification time for all the designed cases. In all the cases, the total cross-sectional area of all fins holds fixed. Initially, the PCM is in a liquid state and its thermal energy is gradually transferred to the cold HTF, which has a lower temperature than the PCM's solidification temperature.

### 4- 1- Effect of fin shape on the discharging process

In this subsection, the influence of the designed fin configuration on the solidification process is compared with those of traditional straight fins as the base case. Fig. 6 represents the PCM liquid fraction contours of two fin configurations at various times. As observed in the figure, at the initial solidification stage, narrow solidified layers of PCM start to form around the fins and HTF tube walls by natural convection heat transfer. As time goes on, the solidification zone gently expands by releasing more heat from the PCM to the cooling boundaries. As time progresses and the solidified layer increases, conduction takes place to further propagate the solid regime. The flow of the liquid PCM is decreased, natural convection becomes insignificant, and conduction heat transfer becomes the predominant mode in discharging process.

It is observed from Fig. 6 that using the new fin configuration significantly improved the PCM solidification rate in comparison to the straight fins. The solid fraction of longitudinal-parabolic fins is greater than that of the straight fins during every time intervals. The higher amount of solidified PCM is due to the more extensive heat transfer surface of the longitudinal-parabolic fin configuration, leading to increased heat removal from the PCM and more expansion of solid layers in the voids between fins. Fig. 7(a) displays the PCM solid fraction against time for two different fin shapes. It is observed that in the initial stage, the solid

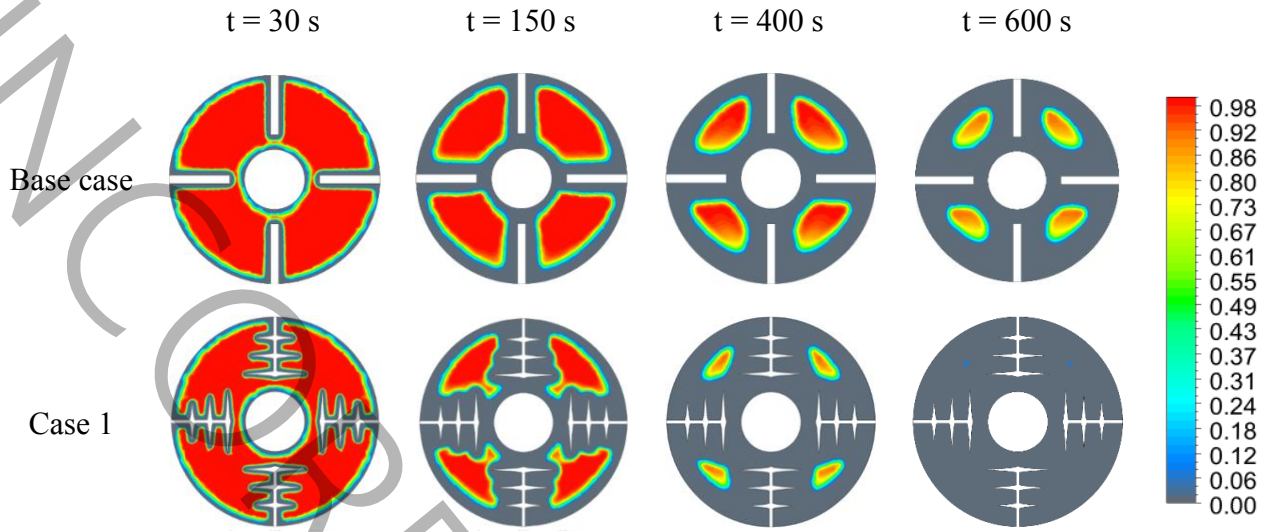


Fig. 6. Contour plot of liquid fraction for the straight fins and longitudinal-parabolic fins.

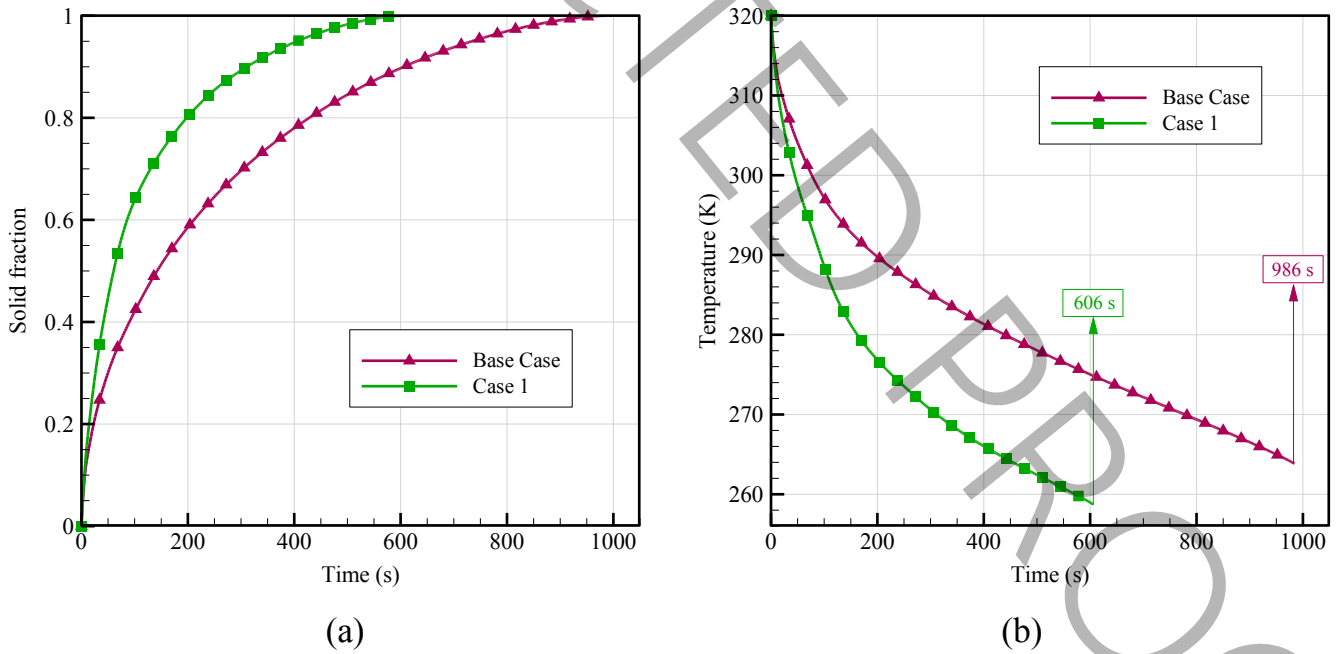
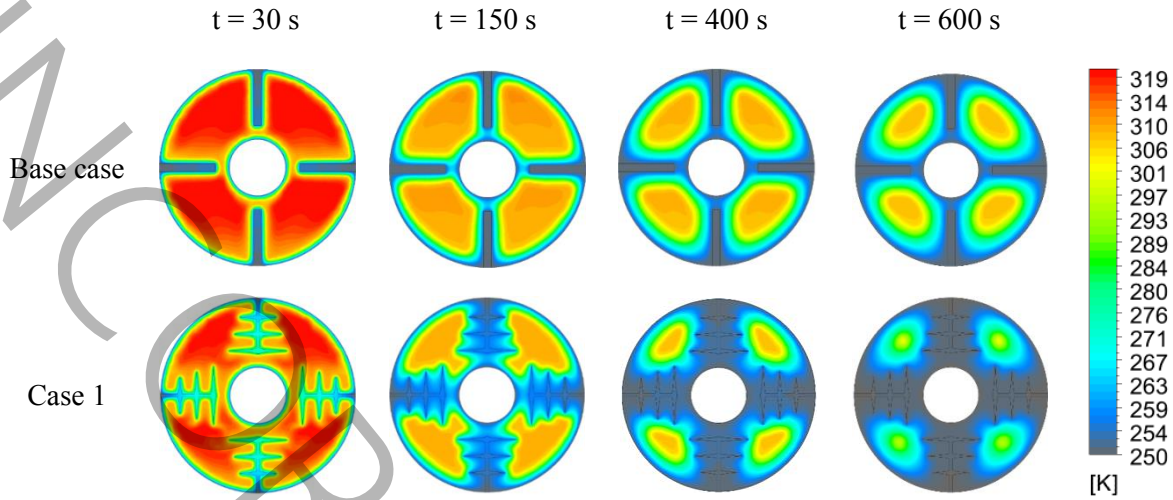


Fig. 7. Comparison of (a) solid fraction and (b) PCM mean temperature over time for the straight fins and longitudinal-parabolic fins.





**Fig. 8. Temperature contours for two different fin shapes.**

fraction increases rapidly due to direct contact of liquid PCM and cold surfaces which facilitates faster heat transfer. As time proceeds and the solidified layer increases, conduction has happened among the solid and its adjacent liquid PCM decelerating the solidification rate owing to the inferior thermal conductivity of PCM. The discharging process of the base case with straight fins is slower than that of Case 1. The discharging time of the conventional straight fins is 986s, while the full solid fraction of longitudinal-parabolic fins is reached within 606s.

Fig. 7(b) illustrates the PCM mean temperature variations over time for two fin shapes. It is observed that the average temperature curve of two cases decreases rapidly at the early stages of the solidification owing to the higher rate of heat transfer caused by a larger temperature gradient. After that, the average temperature curves descend with a decreasing slope by declining the rate of heat transfer as the temperature gradient diminishes. The PCM mean temperature of Case 1 with longitudinal-parabolic fins is lower than that of the straight fins case owing to the different heat transfer behavior of the two cases as explained above.

Fig. 8 shows the temperature contours of two cases at different time intervals. The temperature distribution indicates that the solidification process begins near the cooling walls and penetrates in the PCM. At the initial stages, the temperature of the PCM adjacent to the cooling walls and fins starts to decline till it reaches the PCM liquidus temperature, at which it starts to phase change from liquid to solid state by discharging thermal energy. As the solidification proceeds

and most of the PCM gets solidified, more heat transmission results in the decrease of the PCM mean temperature until it reaches the temperature of the HTF tube's surface. Temperature contours show that the high-temperature regions for the case of straight fins (base case) are more than Case 1 with longitudinal-parabolic fins throughout the discharging process. The temperature reduction in Case 1 is faster than the base case owing to higher thermal penetration depth.

#### 4- 2- Effect of fin radial pitch on the discharging process

Five other longitudinal-parabolic fins with different radial pitches are designed to explore the most effective fin configuration. The fin radial pitches for each case are outlined in Table 2.

Fig. 9 illustrates the liquid fraction contours for various cases. Initially, all Cases have similar solidification patterns with solidified PCM concentrated around the shell walls and fins. As time passes, the solidified zone has expanded to the surroundings of the fins. The main difference is observed at the last stage of the discharging process. Cases 1 and 3 could solidify the PCM faster than other cases and Case 4 is the last to complete the solidification.

Time changes of the PCM solid fraction correspond to different fin radial pitches are displayed in Fig. 10(a). As can be observed, the solidification rates of six cases are almost the same during the initial times. As time goes on, Cases 1 and 3 perform better, and Case 4 lags behind other cases. The full discharging time difference between Case 3 with Case 1 is only 2s. The full discharging time of Case 3 is 608s and that

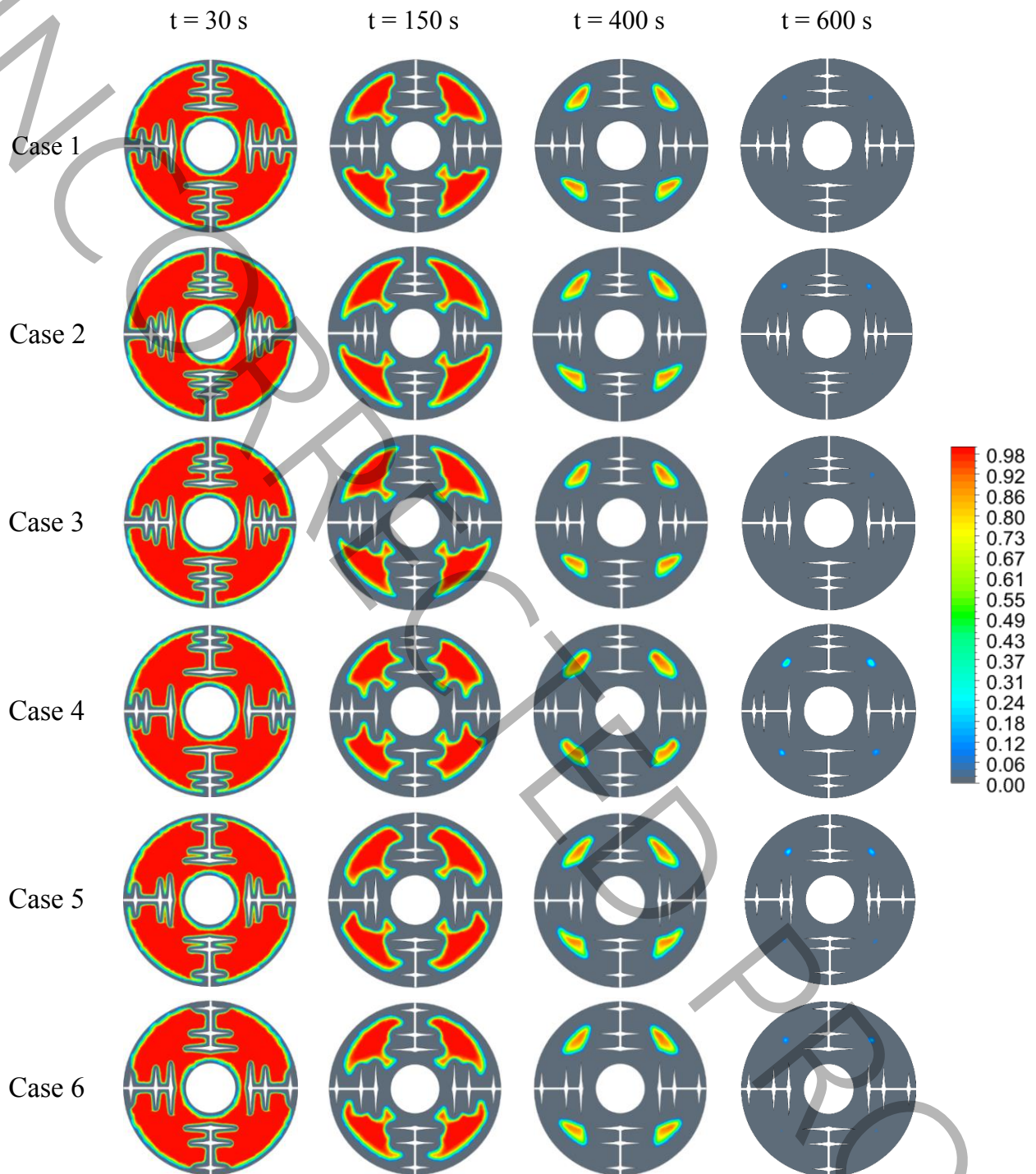


Fig. 9. Liquid fraction contours for different fin radial pitches.

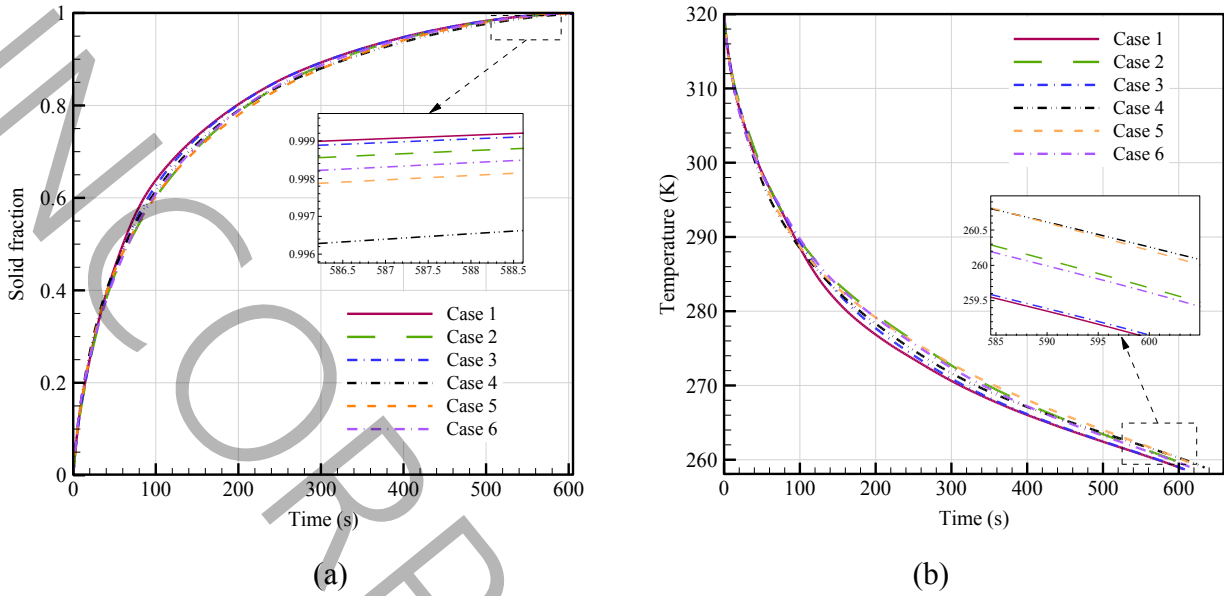


Fig. 10. Comparison of solid fraction (a) and PCM mean temperature (b) over time for different fin radial pitches.

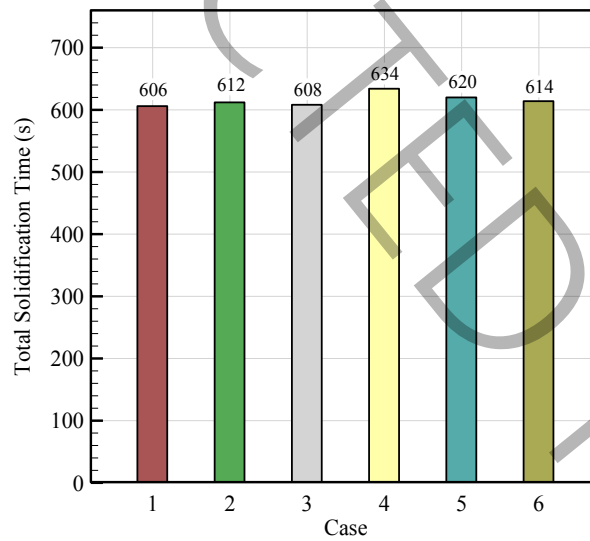
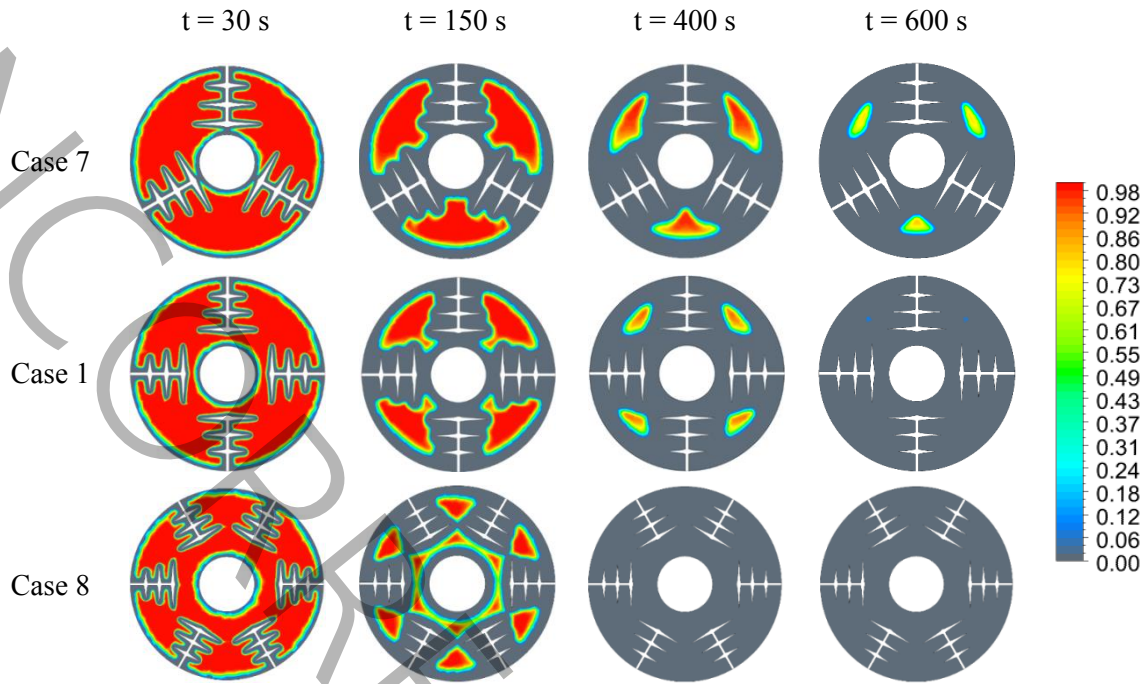


Fig. 11. Solidification times of the cases with various radial pitches.

of Case 4 is 634s. The full solidification time of cases 1-6 is demonstrated in Fig. 11. It is evident that the differences are small.

Fig. 10(b) illustrates the PCM mean temperature evolution for various fin radial pitches. It is observed that the slope of the temperature curves is too steep in the early stages of solidification because of the sensible heat removal from

the PCM. Over time, once the PCM temperature approaches the liquidus temperature, which signifies the point where it starts transforming from liquid to solid state, the slope of the temperature curves reduces for all cases. Once the liquidus temperature is reached, a notable phase change occurs within the PCM by absorbing latent heat. The latent heat absorption moderates the rate of temperature decrease. Accordingly, the



**Fig. 12. Liquid fraction contours for different fin angular pitches.**

temperature decline rate through this stage is slower than the initial phase of the discharging process. As observed in Fig. 10(b), the reduction of temperature in all cases is close to each other. However, Case 1 and Case 3 show a swifter temperature decline during the heat discharging mode.

Since Case 1 could better enhance the discharging efficiency of the LHTES unit among the examined cases with angular pitch of  $90^\circ$ , this case is considered in the following section to explore the impact of fin angular pitch.

#### 4- 3- Effect of fin angular pitch on the discharging process

The influence of angular pitch is also examined to determine the best distribution of the longitudinal-parabolic fins for reducing discharge time. Three different angular pitches are compared while the total cross-sectional area of the fins remains fixed:  $120^\circ$ ,  $90^\circ$  and  $60^\circ$ . Fig. 12 displays the liquid fraction contours for different angular pitches at different times. As can be observed, Case 7 with an angular pitch of  $120^\circ$  has a slower solidification rate than other cases because the fins are spaced further apart. The solidification speed was enhanced by decreasing the angular pitch in Case 1 and Case 8. As the angular pitch decreased from  $120^\circ$  to  $60^\circ$ , the contact heat transfer surface with the PCM increased. At  $t=400s$ , Case 8 has completed solidification in the entire annulus, while Cases 1 and 7 still contain some liquid PCM. Fig. 13(a) indicates the transient evolution of solid fraction for the three angular pitches. It is evident that the solid fraction

of Case 8 is higher than those of Cases 1 and 7 because of improving thermal energy transport through the PCM. Using a fin configuration with a lower angular pitch provides better thermal diffusion and a notable reduction in the PCM discharging time throughout the solidification process.

Fig. 13(b) depicts the change of the PCM mean temperature versus time under various fin angular pitches. It reveals that the angular pitch of fins has a remarkable influence on the temperature distribution and heat transfer characteristics of the PCM. Reducing the angular pitch causes a faster rate of temperature decrease within the PCM. Case 8 (angular pitch of  $60^\circ$ ) completely solidifies after 376s, which is 52.3% less than the time required for Case 7 (angular pitch of  $120^\circ$ ). Fig. 14 displays the temperature contour plots of various angular pitches at different time intervals through the discharging of PCM. The temperature distribution indicates that decreasing the angular pitch accelerates the heat transfer rate owing to a larger contact surface and facilitates heat dissipation from the PCM over time. Case 8 shows the highest temperature drop rate in the whole process, while Case 7 has the lowest one.

#### 4- 4- Comparison of solidification time

The full solidification time for the nine cases is indicated in Fig. 15. The percent reduction in discharging time is represented for the various longitudinal-parabolic fin configurations relative to the straight fin (the base case). It is obvious that the solidification time is decreased for all the

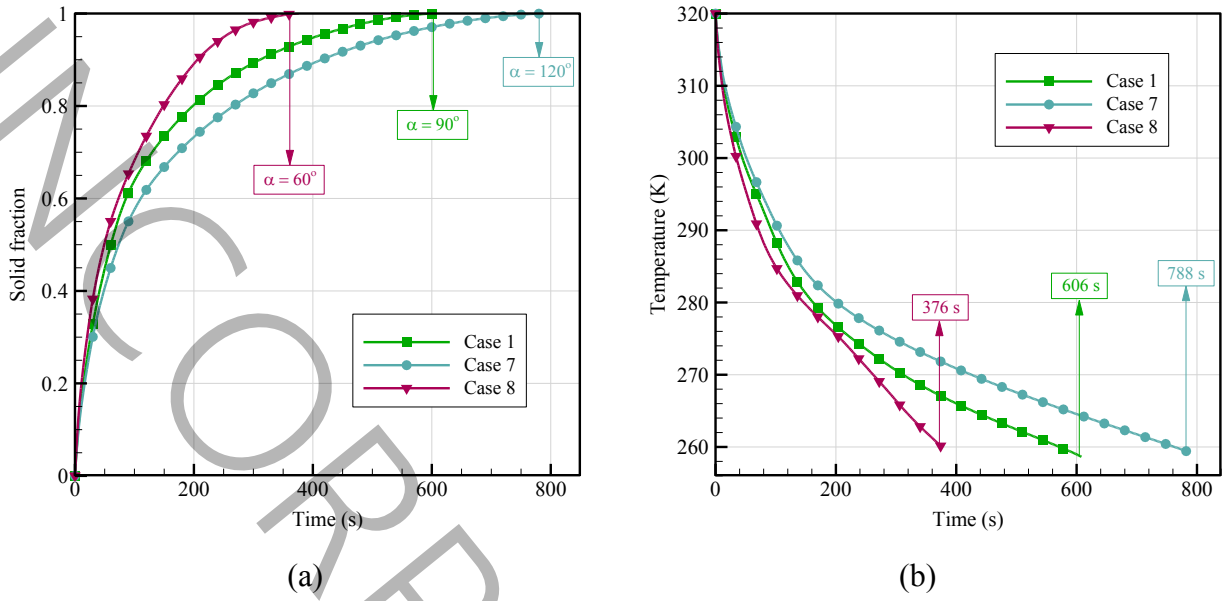


Fig. 13. Comparing the solid fraction (a) and PCM mean temperature (b) over time for different fin angular pitches.

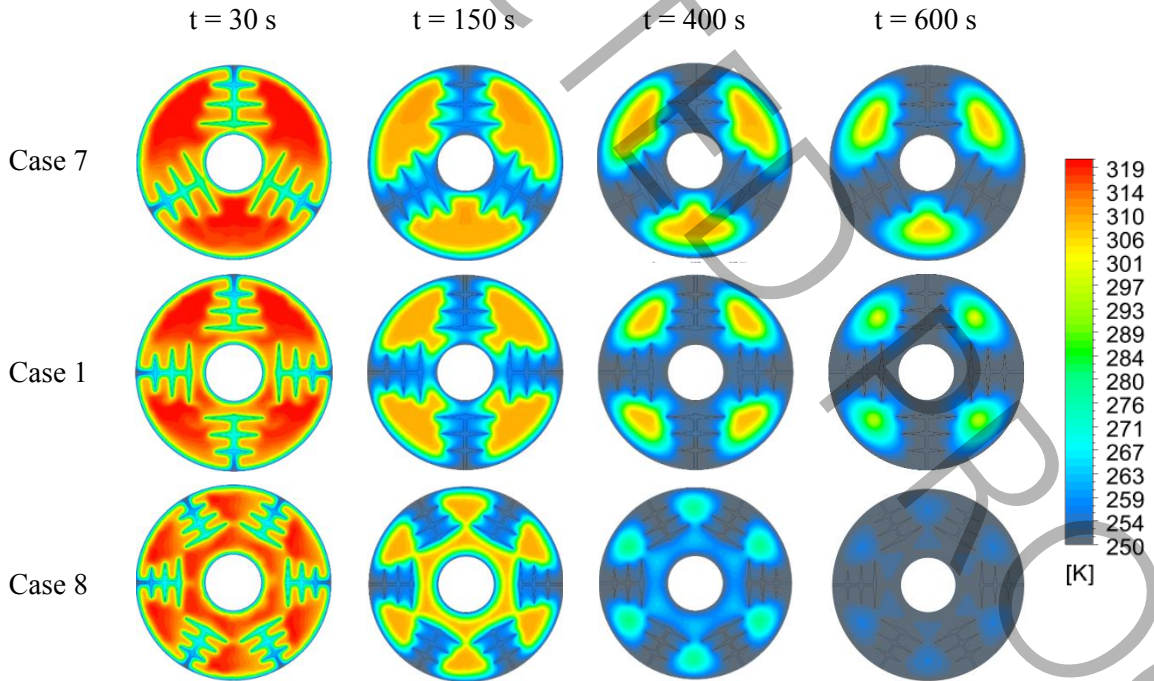
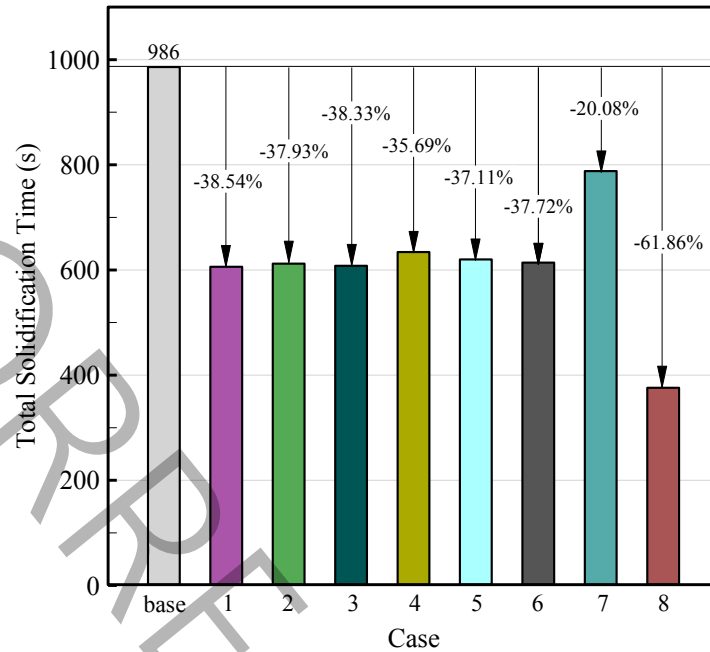


Fig. 14. Temperature contours for different fin angular pitches.



**Fig. 15. Complete solidification time for the nine cases.**

longitudinal-parabolic fin cases in comparison to the straight fin case. For the six different fin radial pitches (Cases 1-6), no significant change in solidification time is observed. However, Case 1 has the minimum discharging time which is 38.54% less than the straight fins case. For the three different fin angular pitches (Case 1-7-8), the full solidification time for Case 8 is minimum which is 37.95% and 52.28% less than Case 1 and Case 7, respectively. Case 8 has the shortest discharging time among the nine cases which is 61.86% less than the base case.

### 5- Conclusion

In the present study, an innovative longitudinal-parabolic fin is embedded into a triplex tube LHTES unit to numerically examine the discharging performance enhancement of PCM. The impacts of geometrical parameters of the designed fin are also investigated to get higher PCM discharging efficiency. The proposed fin is evaluated against the traditional straight fin to reveal its superior thermal performance. Provided that the total surface area of fins holds fixed, several cases with various fin's geometric parameters including radial pitch

and angular pitch are examined to find the most efficient fin design for achieving the highest energy discharge efficiency. The conclusions of the study are summarized as follows:

Compared to the traditional straight fins, the complete solidification time of the triplex tube LHTES system with the longitudinal-parabolic fins declined up to 38.5% which implies that the newly designed fin significantly enhances the PCM discharging rate.

All of the longitudinal-parabolic fin cases with different radial pitches achieve a reduction in energy discharge time. However, the radial pitches of parabolic fins have little impact on the solidification process.

The angular pitch of the longitudinal-parabolic fin has a significant impact on solidification performance, as smaller angular pitches lead to a faster discharging rate. By decreasing the angular pitch from  $120^\circ$  to  $60^\circ$ , the solidification time reduces up to 52.3%.

The maximum saving discharge time for the most efficient longitudinal-parabolic fin design is 61.8% in comparison with straight fins.

## 6- Nomenclature

$A_m$	mushy constant ( $\text{kg.m}^{-3}.\text{s}^{-1}$ )
$C_p$	specific heat at constant pressure ( $\text{J.kg}^{-1}.\text{K}^{-1}$ )
$g$	gravity acceleration ( $\text{m.s}^{-2}$ )
$h$	sensible enthalpy ( $\text{kJ.kg}^{-1}$ )
$H$	total enthalpy ( $\text{kJ.kg}^{-1}$ )
$k$	thermal conductivity ( $\text{W.m}^{-1}.\text{K}^{-1}$ )
$L_f$	latent heat (MJ)
$p$	pressure (Pa)
$S$	momentum source term ( $\text{Pa.m}^{-1}$ )
$t$	time (s)
$T$	temperature (K)
$u$	velocity ( $\text{m.s}^{-1}$ )

## Greek symbols

$\beta$	thermal expansion coefficient ( $\text{K}^{-1}$ )
$\varepsilon$	a small number assigned to prevent division by zero
$\lambda$	melting fraction
$\mu$	viscosity (Pa.s)
$\rho$	density ( $\text{kg.m}^{-3}$ )

## Subscripts

$l$	liquidus of the PCM
$ref$	reference state
$s$	solidus of the PCM

## Abbreviations

HTF	heat transfer fluid
LHTES	latent heat thermal energy storage
PCM	phase change material
QUICK	quadratic upstream interpolation for convective kinematics
SIMPLE	semi-implicit pressure-linked equations

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